

* BIOREACTOR: →

A bioreactor is a device in which a substrate of low value is utilized by living cells to generate a product of higher value.

These are used for food processing, fermentation, waste treatment etc.

On basis of agent used, they are grouped into broad classes:

- i) those based on living cells
- ii) those employing enzymes.

A Bioreactor provide:

- Agitation (for mixing of cells & medium)
- Aeration (for O_2 supply)
- regulation of factors like Temp, pH, pressure, liquid level etc.

Types: → 1) Batch Bioreactor: →

In batch culture, a bioreactor is filled with fresh medium & inoculated. At the end of fermentation, contents are removed for downstream processing.

The reactor is cleaned & sterilized.

It is refilled for next fermentation.

Adv :->

- Reduced risk of contamination
- More flexibility with varying product
- Higher raw material conversion levels

Disad :-> Lower productivity level
Higher cost for labour

2.) Continuous Bioreactor :-> In this, there is continuous inflow of fresh medium & outflow of used medium.

A Spin-filter bioreactor is a good ex. of continuous bioreactor.

Adv :-> Increased potential for automating the process

Decreased toxicity risks to staff

Reduced stress on instruments

Less non-productive time

Disad - Minimal flexibility, Higher investment costs in control & automation equipment.

Higher risk of contamination & cell mutation

TYPES :-> Continuous Cultivation :->

1.) Chemostat :-> In this, medium is pumped continuously & Vol. is constant.

2.) Turbidostat :-> It employs feedback control of pumping rate to maintain a fixed turbidity of the culture.

3.) Auxostat :-> It is method of feeding fresh nutrient based on the concⁿ of metabolic product & related parameter change like pH & diss. O₂.

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- These 3 substrate flow possibilities in packed
 - * Downward flow method
 - * Upward " "
 - * Recycling Method

Air-lift Bioreactor! → Also has tower reactor.
Greater air throughput & higher pressure needed.
It is divided into 3 parts

- Air riser ; downcomer,
- disengagement.

In this no mechanical stirrer & used of agitation is achieved by air bubbles.
These & of closed or batch type but continuous flow reactor & used.

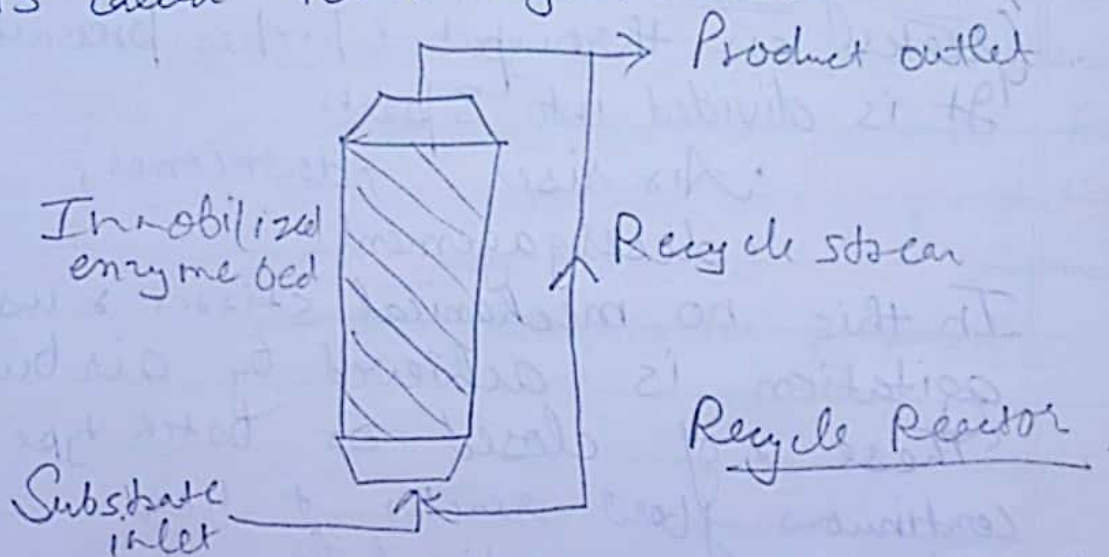
* Adv. over conventional bioreactors.

- Less risks of defects & easier sterilization.
- Large, specific contact area with low energy input
- Well-controlled flow & efficient mixing.

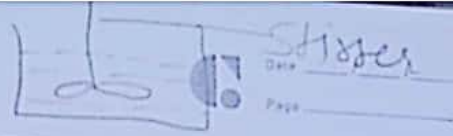
* Disad.!- Higher initial capital investments due to large scale processes

- Lower efficiency of gas compression.
- Inefficient gas separation when foams occur.

Recycled Reactor \Rightarrow It is simply a reactor with recycle system. It is not seen very often, but is very imp. to consider when studying immobilized enzymes. In this, a portion of product stream is recycled & mixed with inlet flow to reactor. If entire product stream is recycled back to inlet stream, then it is called total recycle reactor.



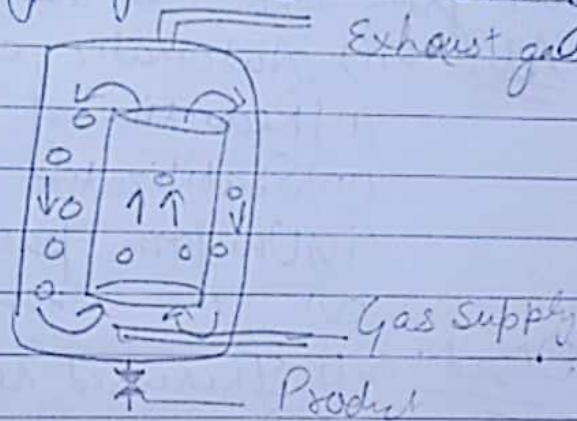
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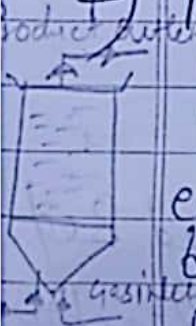
3) Stirred Tank Reactor:- These reactors are simple & consist of tank containing a stirrer & fixed baffles to improve mixing. These are used in batch mode & free enzyme can be employed. Efficient arrangement is provided to maintain temp, pH. It is most common type of aerobic bioreactor in use today.

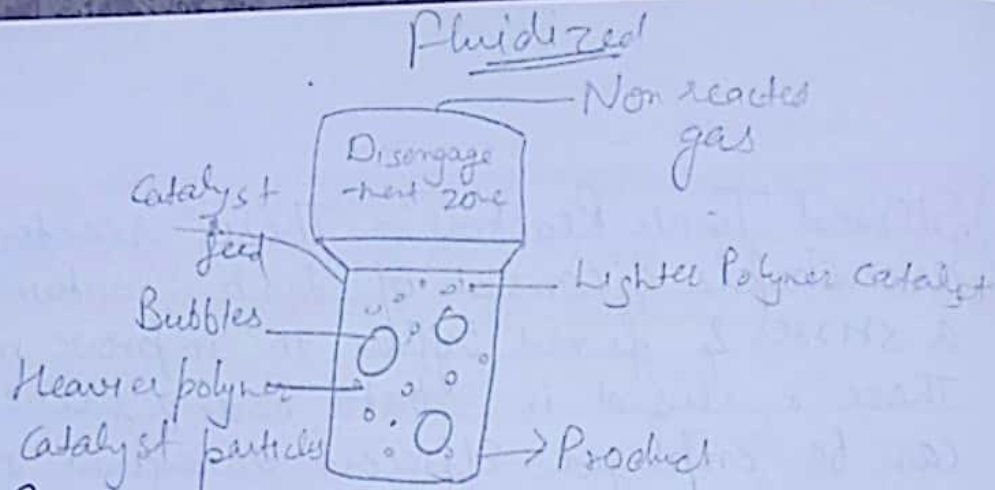
This reactor is useful for substrate solⁿ of high viscosity.

Stirred tank Reactor



4) Fluidized Bed Reactor → It is combination of 2 most packed bed & stirred tank, continuous flow reactors. In these reactors, immobilised enzyme particles are fluidized i.e. the particles become suspended in substrate stream due to flow of substrate stream. In this, substrate is passed upward through the immobilized enzyme bed at high velocity.

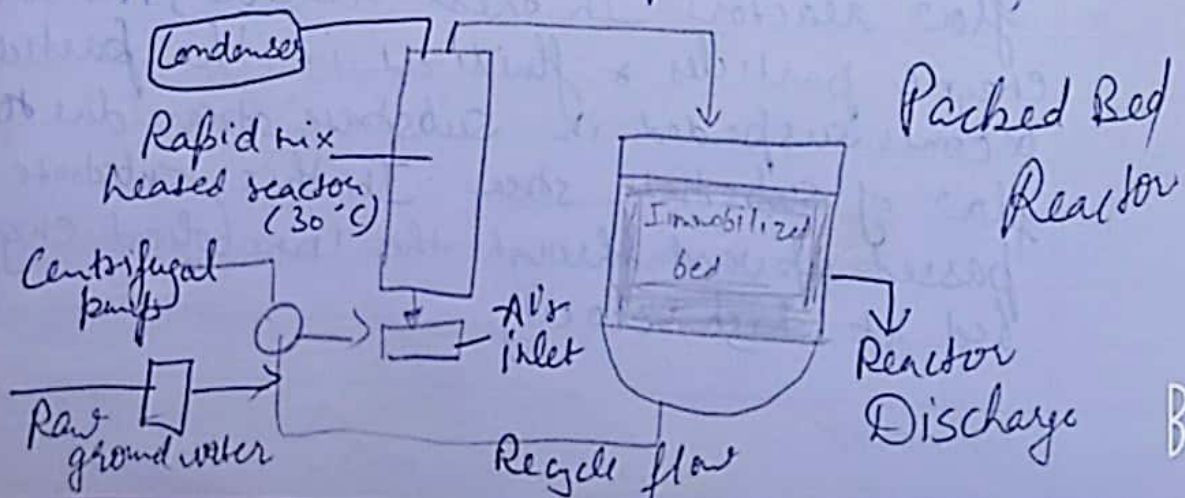




5) Packed Bed Reactor: → These reactors contain a settled bed of immobilized enzyme particles; Reaction mix continuously enters from one end & product moves out from other end. These reactors & like columns.

- Adv! →
- (i) Automatic, easy control & operation.
 - (ii) Reduction of labour costs
 - (iii) Stabilization of operating conditions
 - (iv) Uniform particle mixing.
 - (v) " temp gradients

- Disad! →
- (i) Increased reactor vessel size.
 - (ii) Particle entrainment
 - (iii) Erosion of internal components
 - (iv) Pressure drop



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